## Separation Process Engineering Edition Number 5

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First Printing: 2022

## Corrections for February 14, 2023

| Pg | Error | Correction |
| :--- | :--- | :--- |
| 46 | Eq. (2-59c), Values for C, D, E, F are incorrect. | $\mathrm{C}=-0.179390, \mathrm{D}=-0.012379, \mathrm{E}=-3.86235 \mathrm{E}-04, \mathrm{~F}=-2.955 \mathrm{E}-04$ |
| 49 | Last 3 lines of Part 3 of solution. | For a vertical drum, Eq. (2-59a) with the constants in Eq. <br> $(2-59 \mathrm{c})$ gives Kvertical 0.449, which is high , but agrees with <br> Watkins (1967) charts. |
| 49 | Last line, constant 0.346 and answer. | Constant $=0.449$ and answer is $6.660 \mathrm{ft} / \mathrm{s}$. |
| 50 | $2^{\text {nd }}$ line, value $5.1362 \mathrm{ft} / \mathrm{s}$ and answer 20.57 | Value is $6.660 \mathrm{ft} / \mathrm{s}$ and answer is 15.86 |
| 50 | $3^{\text {rd }}$ line, $\mathrm{D}=5.149 \mathrm{ft}$ | $\mathrm{D}=4.495 \mathrm{ft}$ |


| 50 | $4^{\text {th }}$ line, Round up to 5.5 ft | Round up to the nearest 6 inches, which is a 4.5 ft diameter drum; however, since $\mathrm{K}_{\text {drum }}$ is high and $\mathrm{u}_{\text {perm }}$ is high use of a 5.0 ft diameter drum is recommended. |
| :---: | :---: | :---: |
| 50 | $5^{\text {th }}$ line, $\mathrm{h}_{\text {total }}=4(5.5 \mathrm{ft})=22.0 \mathrm{ft}$ | $\mathrm{h}_{\text {total }}=4(5.0 \mathrm{ft})=20.0 \mathrm{ft}$. |
| 50 | Part E, Check, First 3 lines of Check | The result is close to the result using different equations and constants for $\mathrm{K}_{\text {drum }}$ (Wankat, 2017). Minimums for $\mathrm{h}_{\mathrm{v}}$ and $\mathrm{h}_{\mathrm{f}}$ are |
| 52 |  | Add, Watkins, R. N., "Sizing Separators and Accumulators," Hydrocarbon Processing, 46 (1), 253 (Nov. 1967). |
| 58 | Problem D23, first line: specified a 5.5-foot diameter 22.0-foot long drum | specified a 5.0-foot diameter 20.0-foot long drum |
| 409 | Table 11-9, $2^{\text {nd }}$ column, 3 corrections | the label $5^{\circ} \mathrm{C}$ return $15^{\circ} \mathrm{C}$ should be on line for Chilled water; <br> the label $-20^{\circ} \mathrm{C}$ should be on line for Low T; <br> the label $-50^{\circ} \mathrm{C}$ should be on line for Very low $T$ |
| 536 | Last equation on stage: Value of Per $_{f}$ in denominator $=2.668$ | Value of $\mathrm{Per}_{f}$ in denominator $=2.632$ |
| 1012 | $2^{\text {nd }}$ line. units are $\mathrm{g} / \mathrm{cm}^{3}$ | Units mol/cm ${ }^{3}$ |
| 1034 | Item 18 | After "the toolbar)." add "Feed concentration should be 50 $\mathrm{g} / \mathrm{L}$. |
| 1036 | (lab AC2)Before Answers. Change Turn in to, | Turn in: "Your instructor may request the following assignment. Do breakthrough curves for Dextran T6 and fructose with a feed concentration of $50 \mathrm{~g} / \mathrm{L}$ of each. Use Buds with 50 nodes. For column lengths of 25,50 , and 100 cm use the history to calculate the value of $\mathrm{t}_{\text {mTz }}$, Linear adsorption theory predicts that $\mathrm{t}_{\text {mTZ }}$ is proportional to L to |


|  |  | the 1/2 power. Determine if this prediction is true for <br> Dextran T6." |
| :--- | :--- | :--- |
| 1038 | (Lab AC3) Step 13. Repeat Step 6 | Step 13. Repeat step 9 |
| 1053 | (lab AC8), Specify Table, IP1 $=52744.5$ | IP1 $=52910.3$ |
| 1053 | (lab AC8), Specify Table, IP3 $=3046.7$ | IP3 $=3946.7$ |
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This errata sheet is intended to provide updated technical information. Spelling and grammar misprints are updated during the reprint process, but are not listed on this errata sheet.

